

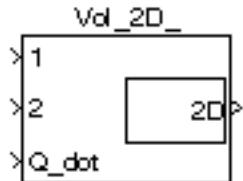
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## **Simulink Report: Vol\_2D\_**

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# Model - Vol\_2D\_



**Tabelle 1.1. Vol\_2D\_ Simulation Parameters**

Solver ode14x	ZeroCross on	StartTime 0.0 StopTime 10.0
RelTol 1e-3	AbsTol auto	Refine 1
InitialStep auto	FixedStep auto	MaxStep auto

**Tabelle 1.2. Vol\_2D\_ Summary Information**

NumModelInputs	N/A	NumModelOutputs	N/A
NumVirtualSubsystems	N/A	NumNonvirtSubsystems	N/A
NumNonVirtBlocksInModel	N/A	NumBlockTypeCounts	N/A
NumBlockSignals	N/A	NumBlockParams	N/A
NumZCEvents	N/A	NumNonsampledZCs	N/A

## Systems

Name	Parent	Snapshot	Blocks	Signals
Vol_2D_	<root>		Vol_2D_	Vol_2D_<1>

## Blocks

Name	Parent	V	P init	T init	X H2O gas init	X CO2 init	X H2O liq init
Vol_2D_	Vol_2D_[1]	NaN	NaN	NaN	NaN	NaN	NaN

**Tabelle 1.3. Block Type Count**

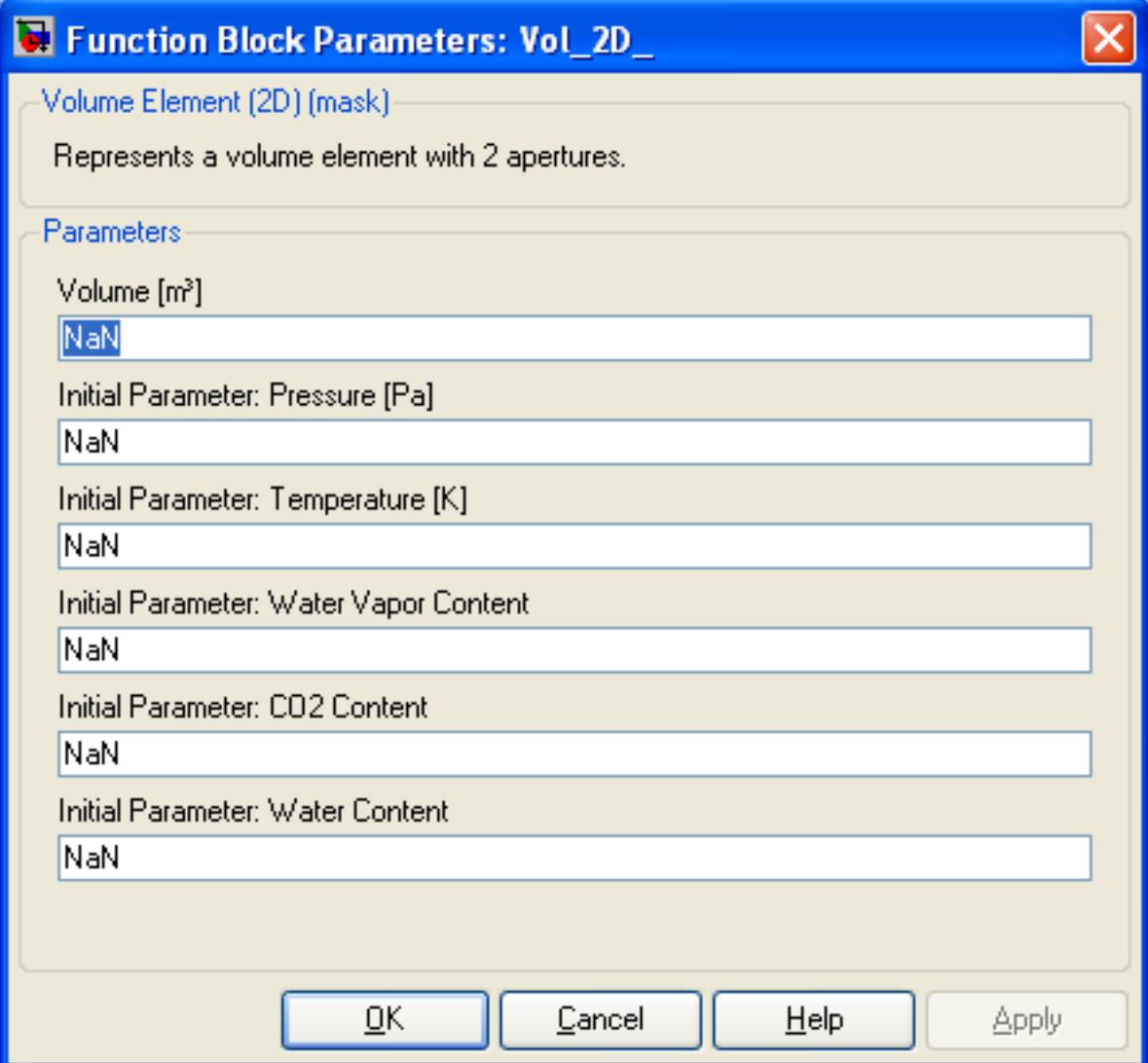
BlockType	Count	Block Names
Import	31	In_1, In_2, Q_dot, V, p_init, T_init, x_H2O_gas_init, x_CO2_init, x_H2O_liq_init, T, m_air, m_H2O_gas,

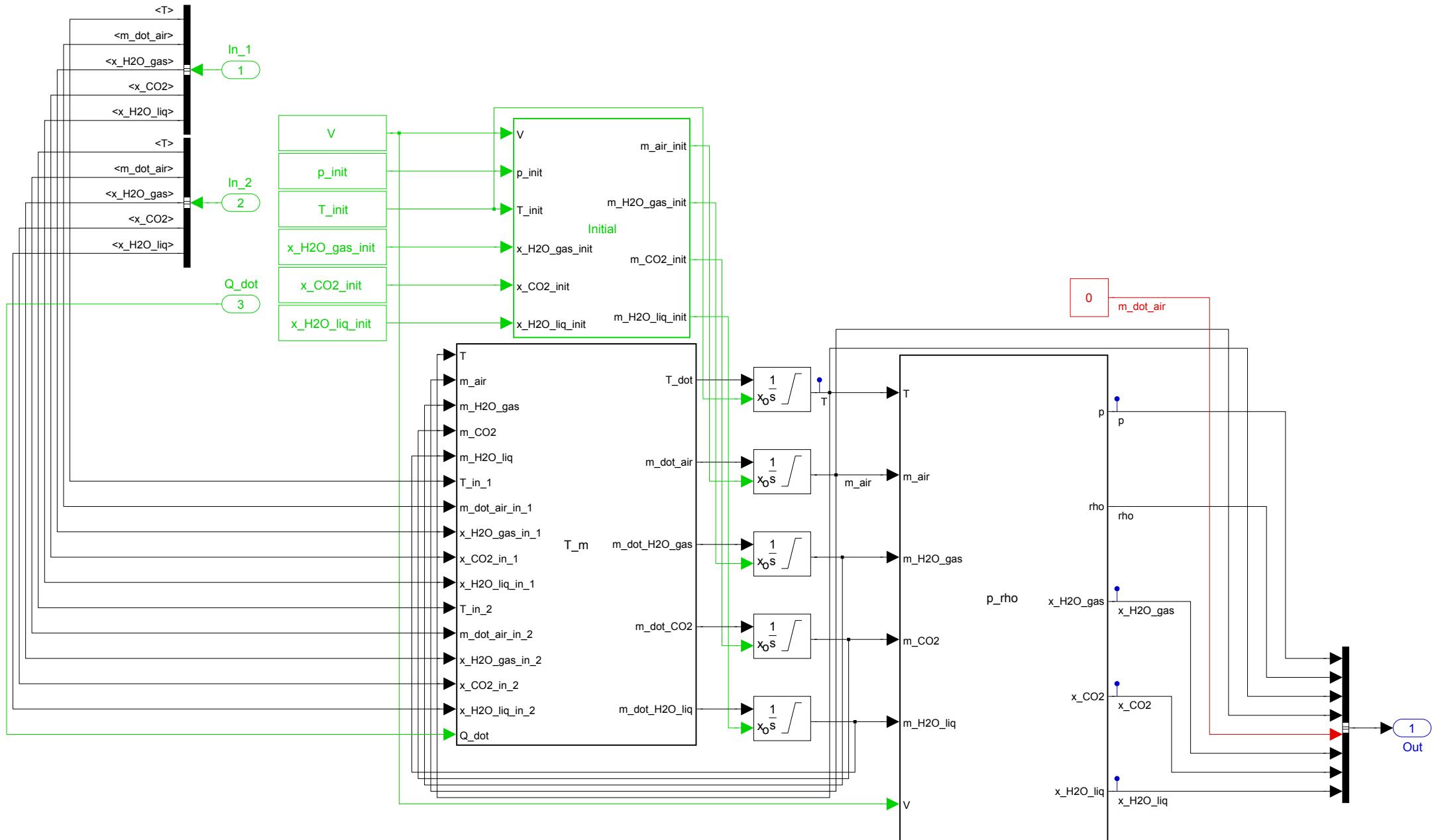
BlockType	Count	Block Names
		m_CO2, m_H2O_liq, T_in_1, m_dot_air_in_1, x_H2O_gas_in_1, x_CO2_in_1, x_H2O_liq_in_1, T_in_2, m_dot_air_in_2, x_H2O_gas_in_2, x_CO2_in_2, x_H2O_liq_in_2, Q_dot, T, m_air, m_H2O_gas, m_CO2, m_H2O_liq, V
Outport	15	m_air_init, m_H2O_gas_init, m_CO2_init, m_H2O_liq_init, T_dot, m_dot_air, m_dot_H2O_gas, m_dot_CO2, m_dot_H2O_liq, p, rho, x_H2O_gas, x_CO2, x_H2O_liq, Out
Constant	7	T_init, V, m_dot_air, p_init, x_CO2_init, x_H2O_gas_init, x_H2O_liq_init
Integrator	5	Integrator1, Integrator2, Integrator3, Integrator4, Integrator5
Terminator	3	Terminator , Terminator , Terminator
Stateflow (m)	3	Embedded MATLAB Function, Embedded_MATLAB_Function_1, Embedded_MATLAB_Function_2
S-Function	3	SFunction , SFunction , SFunction
Demux	3	Demux , Demux , Demux
BusSelector	2	Bus Selector2, Bus Selector5
Volume Element (2D) (m)	1	Vol_2D_-
BusCreator	1	Bus Creator1

## Data and Functions

**Tabelle 1.4. Model Functions**

Function Name	Parent Blocks	Calling string
NaN	Vol_2D_- Vol_2D_- Vol_2D_- Vol_2D_- Vol_2D_- Vol_2D_-	NaN NaN NaN NaN NaN NaN





```
function [m_air_init,m_H2O_gas_init,m_CO2_init,m_H2O_liq_init] = Initial(V,p_init,<
T_init,x_H2O_gas_init,x_CO2_init,x_H2O_liq_init)

% ****
% * Definition of a volume with 2 apertures
% *
% * Number of Inputs:      3
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_2D:
% *
% * Temperature:          T
% * Mass flow dry air:    m_dot_air
% * Content water vapor: x_H2O_gas
% * Content CO2:          x_CO2
% * Content water:        x_H2O_liq
% * External Heat Flow:   Q_dot
% *
% *
% * Relevant output variables of Vol_2D:
% *
% * Pressure:              p
% * Density:               rho
% * Temperature:           T
% * Mass dry air:          m_air
% * Content water vapor:  x_H2O_gas
% * Content CO2:           x_CO2
% * Content water:         x_H2O_liq
% *
% ****
% * Embedded MATLAB Function Initial:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Calculation of the saturation density by a given temperature.
% * 3. Calculation of the saturation mass.
% * 4. Initialisation.
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 2. The saturation density is a function of the temperature. The used
% *    function is described in literature.
% *
% *
% * Last modification : 15.03.2008
% * Author : Christian Müller(HAW)
% *
% ****

% * 1. Definition specific gas constants
R_air          = 287.058;
```

```
R_H2O_gas      = 461.523;
R_CO2          = 188.924;
% ****
%
% * 2. Calculation of the saturation density by a given temperature
rho_H2O_gas_sat = 4.44259*exp(15.05703*(T_init-273.15)/(208.07254+(T_init-273.15)))\n/1000;
% ****
%
% * 3. Calculation of the saturation mass
m_H2O_gas_sat = V*rho_H2O_gas_sat;
% ****
%
% * 4. Initialisation
m_air_init      = p_init*V/(T_init*\n(R_air+x_H2O_gas_init*R_H2O_gas+x_CO2_init*R_CO2));
m_H2O_gas_init   = m_air_init*x_H2O_gas_init;

if m_H2O_gas_init > m_H2O_gas_sat
    m_H2O_gas_init = m_H2O_gas_sat;
    m_air_init     = ((p_init*V/T_init)-(m_H2O_gas_init*R_H2O_gas))/\n(R_air+x_CO2_init*R_CO2);
end

m_CO2_init       = m_air_init*x_CO2_init;
m_H2O_liq_init   = m_air_init*x_H2O_liq_init;
% ****
```

```
function [T_dot,m_dot_air,m_dot_H2O_gas,m_dot_CO2,m_dot_H2O_liq] = T_m(T,m_air,↵
m_H2O_gas,m_CO2,m_H2O_liq,T_in_1,m_dot_air_in_1,x_H2O_gas_in_1,x_CO2_in_1,↵
x_H2O_liq_in_1,T_in_2,m_dot_air_in_2,x_H2O_gas_in_2,x_CO2_in_2,x_H2O_liq_in_2,Q_dot)

% ****
% * Definition of a volume with 2 apertures
% *
% * Number of Inputs:      3
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_2D:
% *
% * Temperature:           T
% * Mass flow dry air:     m_dot_air
% * Content water vapor:   x_H2O_gas
% * Content CO2:            x_CO2
% * Content water:          x_H2O_liq
% * External Heat Flow:    Q_dot
% *
% *
% * Relevant output variables of Vol_2D:
% *
% * Pressure:               p
% * Density:                rho
% * Temperature:             T
% * Mass dry air:            m_air
% * Content water vapor:    x_H2O_gas
% * Content CO2:              x_CO2
% * Content water:            x_H2O_liq
% *
% ****
% * Embedded MATLAB Function T_m:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Redefinition of the input variables.
% * 3. Modification of the mass inside the system.
% * 4. Modification of the temperature inside the system.
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 2. In the case of outgoing mass flow, the characteristic variables of
% *    the mass flow are defined by the state variables of the volume.
% * 3. The increase or decrease of the mass inside the volume is defined
% *    by the incoming (sign: plus) or outgoing (sign: minus) mass flow.
% * 4. The Enthalpy equation of the gas inside the volume is used. the
% *    enthalpy of the liquid water inside the volume is neglected.
% *    Assuming that the liquid water is always in thermal equilibrium with
% *    the gas.
% *
% *
% * Last modification : 15.03.2008
```

```
% * Author : Christian Müller(HAW)
%
% ****
%
% * 1. Definition specific gas constants
R_air           = 287.058;
R_H2O_gas       = 461.523;
R_CO2           = 188.924;
c_p_air          = 1005;
c_p_H2O_gas     = 1870;
c_p_CO2          = 830;
c_v_air          = c_p_air-R_air;
c_v_H2O_gas     = c_p_H2O_gas-R_H2O_gas;
c_v_CO2          = c_p_CO2-R_CO2;
%
% ****
%
% * 2. Redefinition of the input variables
if m_dot_air_in_1 < 0
    T_in_1      = T;
    m_dot        = m_dot_air_in_1*(1+x_H2O_gas_in_1+x_CO2_in_1);
    m_dot_air_in_1 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));
    x_H2O_gas_in_1 = (m_H2O_gas/m_air);
    x_CO2_in_1   = (m_CO2/m_air);
    x_H2O_liq_in_1 = (m_H2O_liq/m_air);
end

if m_dot_air_in_2 < 0
    T_in_2      = T;
    m_dot        = m_dot_air_in_2*(1+x_H2O_gas_in_2+x_CO2_in_2);
    m_dot_air_in_2 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));
    x_H2O_gas_in_2 = (m_H2O_gas/m_air);
    x_CO2_in_2   = (m_CO2/m_air);
    x_H2O_liq_in_2 = (m_H2O_liq/m_air);
end
%
% ****
%
% * 3. Modification of the mass inside the system
m_dot_air        = m_dot_air_in_1+m_dot_air_in_2;
m_dot_H2O_gas    = m_dot_air_in_1*x_H2O_gas_in_1+m_dot_air_in_2*x_H2O_gas_in_2;
m_dot_CO2         = m_dot_air_in_1*x_CO2_in_1+m_dot_air_in_2*x_CO2_in_2;
m_dot_H2O_liq    = m_dot_air_in_1*x_H2O_liq_in_1+m_dot_air_in_2*x_H2O_liq_in_2;
%
% ****
%
% * 4. Modification of the temperature inside the system
T_dot            = (Q_dot+m_dot_air_in_1*(c_p_air*T_in_1-c_v_air*T)+m_dot_air_in_2*(c_p_air*T_in_2-c_v_air*T)+m_dot_air_in_1*x_H2O_gas_in_1*(c_p_H2O_gas*T_in_1-c_v_H2O_gas*T)+m_dot_air_in_2*x_H2O_gas_in_2*(c_p_H2O_gas*T_in_2-c_v_H2O_gas*T)+m_dot_air_in_1*x_CO2_in_1*(c_p_CO2*T_in_1-c_v_CO2*T)+m_dot_air_in_2*x_CO2_in_2*(c_p_CO2*T_in_2-c_v_CO2*T))/(c_v_air*m_air+c_v_H2O_gas*m_H2O_gas+c_v_CO2*m_CO2);
%
% ****
```

```
function [p,rho,x_H2O_gas,x_CO2,x_H2O_liq] = p_rho(T,m_air,m_H2O_gas,m_CO2,m_H2O_liq,V)

% ****
% * Definition of a volume with 2 apertures
% *
% * Number of Inputs:      3
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_2D:
% *
% * Temperature:           T
% * Mass flow dry air:     m_dot_air
% * Content water vapor:   x_H2O_gas
% * Content CO2:            x_CO2
% * Content water:          x_H2O_liq
% * External Heat Flow:    Q_dot
% *
% *
% * Relevant output variables of Vol_2D:
% *
% * Pressure:               p
% * Density:                rho
% * Temperature:             T
% * Mass dry air:            m_air
% * Content water vapor:    x_H2O_gas
% * Content CO2:              x_CO2
% * Content water:            x_H2O_liq
% *
% ****
% * Embedded MATLAB Function p_rho:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Calculation of the density.
% * 3. Calculation of the pressure.
% * 4. Calculation of the water vapor content, CO2 content and
% *    water content.
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 4. The differnt contents are defined in respect of the mass of the
% *    dry air.
% *
% *
% * Last modification : 15.03.2008
% * Author : Christian Müller(HAW)
% *
% ****

% * 1. Definition specific gas constants
R_air      = 287.058;
R_H2O_gas = 461.523;
```

```
R_CO2      = 188.924;
% ****
%
% * 2. Calculation of the density
rho       = (m_air+m_H2O_gas+m_CO2)/V;
% ****
%
% * 3. Calculation of the pressure
p         = T*(m_air*R_air+m_H2O_gas*R_H2O_gas+m_CO2*R_CO2)/V;
% ****
%
% * 4. Calculation of the water vapor content, CO2 content and
% *      water content
x_H2O_gas = m_H2O_gas/m_air;
x_CO2     = m_CO2/m_air;
x_H2O_liq = m_H2O_liq/m_air;
% ****
```