

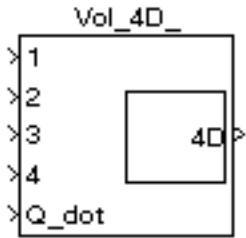
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## **Simulink Report: Vol\_4D\_**

Christian Müller

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# Model - Vol\_4D\_



**Tabelle 1.1. Vol\_4D\_ Simulation Parameters**

Solver ode14x	ZeroCross on	StartTime 0.0 StopTime 10.0
RelTol 1e-3	AbsTol auto	Refine 1
InitialStep auto	FixedStep auto	MaxStep auto

**Tabelle 1.2. Vol\_4D\_ Summary Information**

NumModelInputs	N/A	NumModelOutputs	N/A
NumVirtualSubsystems	N/A	NumNonvirtSubsystems	N/A
NumNonVirtBlocksInModel	N/A	NumBlockTypeCounts	N/A
NumBlockSignals	N/A	NumBlockParams	N/A
NumZCEvents	N/A	NumNonsampledZCs	N/A

## Systems

Name	Parent	Snapshot	Blocks	Signals
Vol_4D_	<root>	<pre> graph LR     Vol4D[Vol_4D_] ---&gt;1     Vol4D ---&gt;2     Vol4D ---&gt;3     Vol4D ---&gt;4     Vol4D ---&gt;Qdot[&gt;Q_dot]     Vol4D ---&gt;     subgraph Inside [4D]         direction TB         4D[4D]     end     &gt;1 --- Inside     &gt;2 --- Inside     &gt;3 --- Inside     &gt;4 --- Inside     &gt;Qdot --- Inside     &gt; --- Inside </pre>	Vol_4D_	Vol_4D_<1>

## Blocks

Name	Parent	V	P init	T init	X H2O gas init	X CO2 init	X H2O liq init
Vol_4D_	Vol_4D_[1]	NaN	NaN	NaN	NaN	NaN	NaN

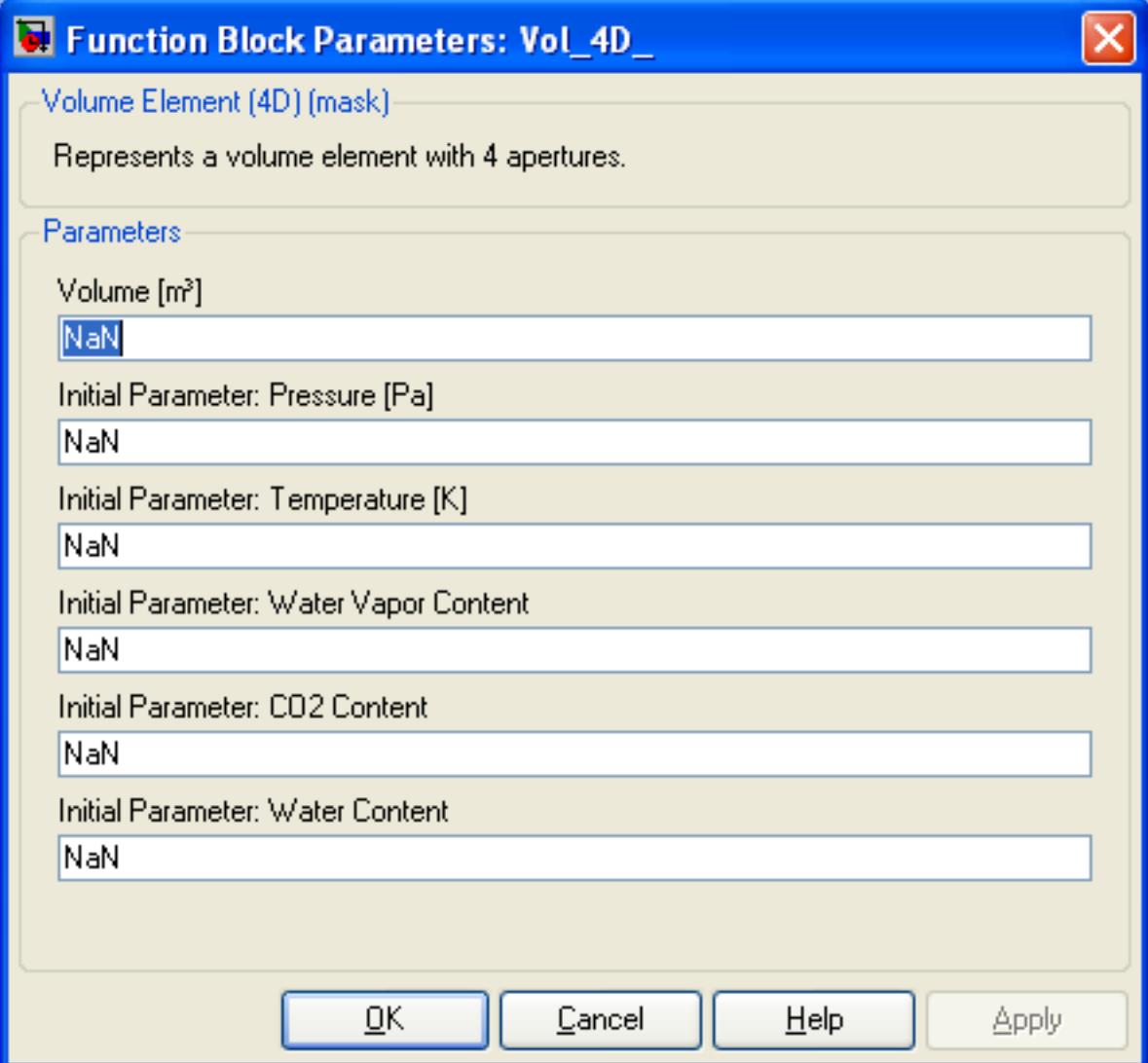
**Tabelle 1.3. Block Type Count**

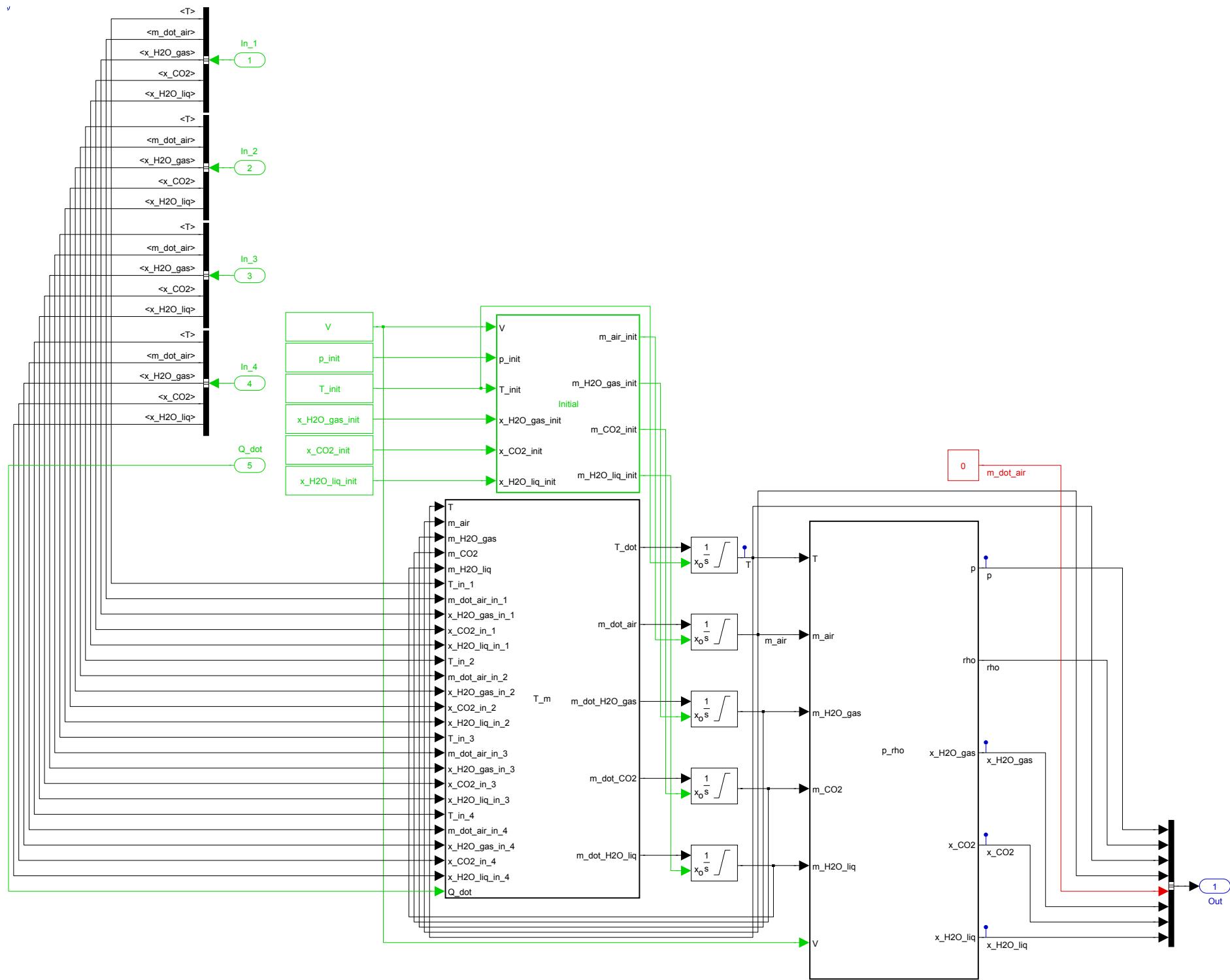
BlockType	Count	Block Names
Import	43	In_1, In_2, In_3, In_4, Q_dot, V, p_init, T_init, x_H2O_gas_init, x_CO2_init, x_H2O_liq_init, T, m_air, m_H2O_gas, m_CO2, m_H2O_liq, T_in_1, m_dot_air_in_1, x_H2O_gas_in_1, x_CO2_in_1, x_H2O_liq_in_1, T_in_2, m_dot_air_in_2, x_H2O_gas_in_2, x_CO2_in_2, x_H2O_liq_in_2, T_in_3, m_dot_air_in_3, x_H2O_gas_in_3, x_CO2_in_3, x_H2O_liq_in_3, T_in_4, m_dot_air_in_4, x_H2O_gas_in_4, x_CO2_in_4, x_H2O_liq_in_4, Q_dot, T, m_air, m_H2O_gas, m_CO2, m_H2O_liq, V
Outport	15	m_air_init, m_H2O_gas_init, m_CO2_init, m_H2O_liq_init, T_dot, m_dot_air, m_dot_H2O_gas, m_dot_CO2, m_dot_H2O_liq, p, rho, x_H2O_gas, x_CO2, x_H2O_liq, Out
Constant	7	T_init, V, m_dot_air, p_init, x_CO2_init, x_H2O_gas_init, x_H2O_liq_init
Integrator	5	Integrator1, Integrator2, Integrator3, Integrator4, Integrator5
BusSelector	4	Bus Selector1, Bus Selector2, Bus Selector3, Bus Selector5
Terminator	3	Terminator , Terminator , Terminator
Stateflow (m)	3	Embedded MATLAB Function, Embedded_MATLAB_Function_1, Embedded_MATLAB_Function_2
S-Function	3	SFunction , SFunction , SFunction
Demux	3	Demux , Demux , Demux
Volume Element (4D) (m)	1	Vol_4D_-
BusCreator	1	Bus Creator1

## Data and Functions

**Tabelle 1.4. Model Functions**

Function Name	Parent Blocks	Calling string
NaN	Vol_4D_- Vol_4D_- Vol_4D_- Vol_4D_- Vol_4D_- Vol_4D_-	NaN NaN NaN NaN NaN NaN





```
function [m_air_init,m_H2O_gas_init,m_CO2_init,m_H2O_liq_init] = Initial(V,p_init,<
T_init,x_H2O_gas_init,x_CO2_init,x_H2O_liq_init)

% ****
% * Definition of a volume with 4 apertures
% *
% * Number of Inputs:      5
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_4D:
% *
% * Temperature:          T
% * Mass flow dry air:    m_dot_air
% * Content water vapor: x_H2O_gas
% * Content CO2:          x_CO2
% * Content water:        x_H2O_liq
% * External Heat Flow:   Q_dot
% *
% *
% * Relevant output variables of Vol_4D:
% *
% * Pressure:              p
% * Density:               rho
% * Temperature:           T
% * Mass dry air:          m_air
% * Content water vapor:  x_H2O_gas
% * Content CO2:           x_CO2
% * Content water:         x_H2O_liq
% *
% ****
% * Embedded MATLAB Function Initial:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Calculation of the saturation density by a given temperature.
% * 3. Calculation of the saturation mass.
% * 4. Initialisation.
% *
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 2. The saturation density is a function of the temperature. The used
% *    function is described in literature.
% *
% *
% * Last modification : 15.03.2008
% * Author : Christian Müller(HAW)
% *
% ****

% * 1. Definition specific gas constants
R_air          = 287.058;
```

```
R_H2O_gas      = 461.523;
R_CO2          = 188.924;
% ****
%
% * 2. Calculation of the saturation density by a given temperature
rho_H2O_gas_sat = 4.44259*exp(15.05703*(T_init-273.15)/(208.07254+(T_init-273.15)))\n/1000;
% ****
%
% * 3. Calculation of the saturation mass
m_H2O_gas_sat = V*rho_H2O_gas_sat;
% ****
%
% * 4. Initialisation
m_air_init     = p_init*V/(T_init*\n(R_air+x_H2O_gas_init*R_H2O_gas+x_CO2_init*R_CO2));
m_H2O_gas_init = m_air_init*x_H2O_gas_init;

if m_H2O_gas_init > m_H2O_gas_sat
    m_H2O_gas_init = m_H2O_gas_sat;
    m_air_init     = ((p_init*V/T_init)-(m_H2O_gas_init*R_H2O_gas))/\n(R_air+x_CO2_init*R_CO2);
end

m_CO2_init      = m_air_init*x_CO2_init;
m_H2O_liq_init  = m_air_init*x_H2O_liq_init;
% ****
```

```
function [T_dot,m_dot_air,m_dot_H2O_gas,m_dot_CO2,m_dot_H2O_liq] = T_m(T,m_air,%
m_H2O_gas,m_CO2,m_H2O_liq,T_in_1,m_dot_air_in_1,x_H2O_gas_in_1,x_CO2_in_1,%
x_H2O_liq_in_1,T_in_2,m_dot_air_in_2,x_H2O_gas_in_2,x_CO2_in_2,x_H2O_liq_in_2,T_in_3,%
m_dot_air_in_3,x_H2O_gas_in_3,x_CO2_in_3,x_H2O_liq_in_3,T_in_4,m_dot_air_in_4,%
x_H2O_gas_in_4,x_CO2_in_4,x_H2O_liq_in_4,Q_dot)

% ****
% * Definition of a volume with 4 apertures
% *
% * Number of Inputs:      5
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_4D:
% *
% * Temperature:          T
% * Mass flow dry air:    m_dot_air
% * Content water vapor:  x_H2O_gas
% * Content CO2:          x_CO2
% * Content water:        x_H2O_liq
% * External Heat Flow:   Q_dot
% *
% *
% * Relevant output variables of Vol_4D:
% *
% * Pressure:              p
% * Density:               rho
% * Temperature:           T
% * Mass dry air:          m_air
% * Content water vapor:   x_H2O_gas
% * Content CO2:            x_CO2
% * Content water:          x_H2O_liq
% *
% ****
% * Embedded MATLAB Function T_m:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Modification of the mass inside the system.
% * 3. Redefinition of the input variables.
% * 4. Modification of the temperature inside the system.
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 2. The increase or decrease of the mass inside the volume is defined
% *    by the incoming (sign: plus) or outgoing (sign: minus) mass flow.
% * 3. In the case of outgoing mass flow, the characteristic variables of
% *    the mass flow are defined by the state variables of the volume.
% * 4. The Enthalpy equation of the gas inside the volume is used. the
% *    enthalpy of the liquid water inside the volume is neglected.
% *    Assuming that the liquid water is always in thermal equilibrium with
% *    the gas.
```

```
% *  
% * Last modification : 15.03.2008  
% * Author : Christian Müller(HAW)  
% *  
% *****  
  
% * 1. Definition specific gas constants  
R_air = 287.058;  
R_H2O_gas = 461.523;  
R_CO2 = 188.924;  
c_p_air = 1005;  
c_p_H2O_gas = 1870;  
c_p_CO2 = 830;  
c_v_air = c_p_air-R_air;  
c_v_H2O_gas = c_p_H2O_gas-R_H2O_gas;  
c_v_CO2 = c_p_CO2-R_CO2;  
% *****  
  
% * 2. Redefinition of the input variables  
if m_dot_air_in_1 < 0  
    T_in_1 = T;  
    m_dot = m_dot_air_in_1*(1+x_H2O_gas_in_1+x_CO2_in_1);  
    m_dot_air_in_1 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));  
    x_H2O_gas_in_1 = (m_H2O_gas/m_air);  
    x_CO2_in_1 = (m_CO2/m_air);  
    x_H2O_liq_in_1 = (m_H2O_liq/m_air);  
end  
  
if m_dot_air_in_2 < 0  
    T_in_2 = T;  
    m_dot = m_dot_air_in_2*(1+x_H2O_gas_in_2+x_CO2_in_2);  
    m_dot_air_in_2 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));  
    x_H2O_gas_in_2 = (m_H2O_gas/m_air);  
    x_CO2_in_2 = (m_CO2/m_air);  
    x_H2O_liq_in_2 = (m_H2O_liq/m_air);  
end  
  
if m_dot_air_in_3 < 0  
    T_in_3 = T;  
    m_dot = m_dot_air_in_3*(1+x_H2O_gas_in_3+x_CO2_in_3);  
    m_dot_air_in_3 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));  
    x_H2O_gas_in_3 = (m_H2O_gas/m_air);  
    x_CO2_in_3 = (m_CO2/m_air);  
    x_H2O_liq_in_3 = (m_H2O_liq/m_air);  
end  
  
if m_dot_air_in_4 < 0  
    T_in_4 = T;  
    m_dot = m_dot_air_in_4*(1+x_H2O_gas_in_4+x_CO2_in_4);  
    m_dot_air_in_4 = m_dot*(1/(1+(m_H2O_gas/m_air)+(m_CO2/m_air)));  
    x_H2O_gas_in_4 = (m_H2O_gas/m_air);  
    x_CO2_in_4 = (m_CO2/m_air);  
    x_H2O_liq_in_4 = (m_H2O_liq/m_air);  
end  
% *****
```

```
% * 3. Modification of the mass inside the system
m_dot_air      = m_dot_air_in_1+m_dot_air_in_2+m_dot_air_in_3+m_dot_air_in_4;
m_dot_H2O_gas  = ↵
m_dot_air_in_1*x_H2O_gas_in_1+m_dot_air_in_2*x_H2O_gas_in_2+m_dot_air_in_3*x_H2O_gas_in_3+↵
_m_dot_air_in_4*x_H2O_gas_in_4;
m_dot_CO2      = ↵
m_dot_air_in_1*x_CO2_in_1+m_dot_air_in_2*x_CO2_in_2+m_dot_air_in_3*x_CO2_in_3+m_dot_air_in_4*x_CO2_in_4;
m_dot_H2O_liq  = ↵
m_dot_air_in_1*x_H2O_liq_in_1+m_dot_air_in_2*x_H2O_liq_in_2+m_dot_air_in_3*x_H2O_liq_in_3+↵
_m_dot_air_in_4*x_H2O_liq_in_4;
% ****
%
% * 4. Modification of the temperature inside the system
T_dot          = (Q_dot+m_dot_air_in_1*(c_p_air*T_in_1-c_v_air*T)+m_dot_air_in_2*↵
(c_p_air*T_in_2-c_v_air*T)+m_dot_air_in_3*(c_p_air*T_in_3-c_v_air*T)+m_dot_air_in_4*↵
(c_p_air*T_in_4-c_v_air*T)+m_dot_air_in_1*x_H2O_gas_in_1*(c_p_H2O_gas*T_in_1-↵
c_v_H2O_gas*T)+m_dot_air_in_2*x_H2O_gas_in_2*(c_p_H2O_gas*T_in_2-c_v_H2O_gas*T) ↵
+m_dot_air_in_3*x_H2O_gas_in_3*(c_p_H2O_gas*T_in_3-c_v_H2O_gas*T) ↵
+m_dot_air_in_4*x_H2O_gas_in_4*(c_p_H2O_gas*T_in_4-c_v_H2O_gas*T) ↵
+m_dot_air_in_1*x_CO2_in_1*(c_p_CO2*T_in_1-c_v_CO2*T)+m_dot_air_in_2*x_CO2_in_2*↵
(c_p_CO2*T_in_2-c_v_CO2*T)+m_dot_air_in_3*x_CO2_in_3*(c_p_CO2*T_in_3-c_v_CO2*T) ↵
+m_dot_air_in_4*x_CO2_in_4*(c_p_CO2*T_in_4-c_v_CO2*T))/ ↵
(c_v_air*m_air+c_v_H2O_gas*m_H2O_gas+c_v_CO2*m_CO2);
% ****
```

```
function [p,rho,x_H2O_gas,x_CO2,x_H2O_liq] = p_rho(T,m_air,m_H2O_gas,m_CO2,m_H2O_liq,V)

% ****
% * Definition of a volume with 4 apertures
% *
% * Number of Inputs:      5
% *
% * Parameter : Volume:    V
% *
% *
% * Relevant input variables of Vol_4D:
% *
% * Temperature:           T
% * Mass flow dry air:     m_dot_air
% * Content water vapor:   x_H2O_gas
% * Content CO2:            x_CO2
% * Content water:          x_H2O_liq
% * External Heat Flow:    Q_dot
% *
% *
% * Relevant output variables of Vol_4D:
% *
% * Pressure:               p
% * Density:                rho
% * Temperature:             T
% * Mass dry air:            m_air
% * Content water vapor:    x_H2O_gas
% * Content CO2:              x_CO2
% * Content water:            x_H2O_liq
% *
% ****
% * Embedded MATLAB Function p_rho:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Calculation of the density.
% * 3. Calculation of the pressure.
% * 4. Calculation of the water vapor content, CO2 content and
% *    water content.
% *
% *
% * Assumptions:
% * 1. The gas mixture inside the volume consists of water vapor (H2O_gas),
% *    CO2 and water (H2O_liq, state: fog).
% * 4. The differnt contents are defined in respect of the mass of the
% *    dry air.
% *
% *
% * Last modification : 15.03.2008
% * Author : Christian Müller(HAW)
% *
% ****

% * 1. Definition specific gas constants
R_air      = 287.058;
R_H2O_gas = 461.523;
```

```
R_CO2      = 188.924;
% ****
%
% * 2. Calculation of the density
rho        = (m_air+m_H2O_gas+m_CO2)/V;
% ****
%
% * 3. Calculation of the pressure
p          = T*(m_air*R_air+m_H2O_gas*R_H2O_gas+m_CO2*R_CO2)/V;
% ****
%
% * 4. Calculation of the water vapor content, CO2 content and
% *      water content
x_H2O_gas = m_H2O_gas/m_air;
x_CO2     = m_CO2/m_air;
x_H2O_liq = m_H2O_liq/m_air;
% ****
```