

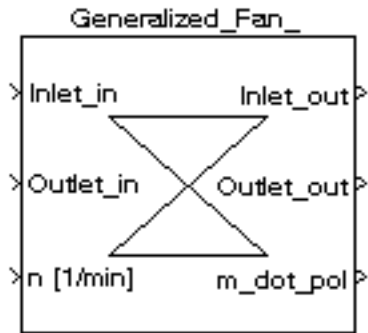
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# **Simulink Report: Generalized\_Fan\_**

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# Model - Generalized\_Fan\_



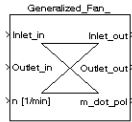
**Tabelle 1.1. Generalized\_Fan\_ Simulation Parameters**

<i>Solver</i> ode14x	<i>ZeroCross</i> on	<i>StartTime</i> 0.0 <i>StopTime</i> 10.0
<i>RelTol</i> 1e-3	<i>AbsTol</i> auto	<i>Refine</i> 1
<i>InitialStep</i> auto	<i>FixedStep</i> auto	<i>MaxStep</i> auto

**Tabelle 1.2. Generalized\_Fan\_ Summary Information**

<i>NumModelInputs</i>	N/A	<i>NumModelOutputs</i>	N/A
<i>NumVirtualSubsystems</i>	N/A	<i>NumNonvirtSubsystems</i>	N/A
<i>NumNonVirtBlocksInModel</i>	N/A	<i>NumBlockTypeCounts</i>	N/A
<i>NumBlockSignals</i>	N/A	<i>NumBlockParams</i>	N/A
<i>NumZCEvents</i>	N/A	<i>NumNonsampledZCs</i>	N/A

## Systems



Name	Parent	Snapshot	Blocks	Signals
Generalized_Fan_	<root>		Generalized_Fan_	Generalized_Fan_<1> Generalized_Fan_<2> Generalized_Fan_<3>

## Blocks

**Tabelle 1.3. Block Type Count**

BlockType	Count	Block Names
Inport	22	Inlet_In, Outlet_In, n, n, n_0, n_min, rho_0, a_0, a_1, a_2, a_3, V_dot_limit, K, p_in, rho_in, T_in, x_H2O_gas_in,



 **Function Block Parameters: Generalized\_Fan\_** 

Subsystem (mask)

Parameters

Diameter [m]

Reference: Rotational Speed [1/min]

Lower Limit: Rotational Speed [1/min]

Reference: Density [kg/m³]

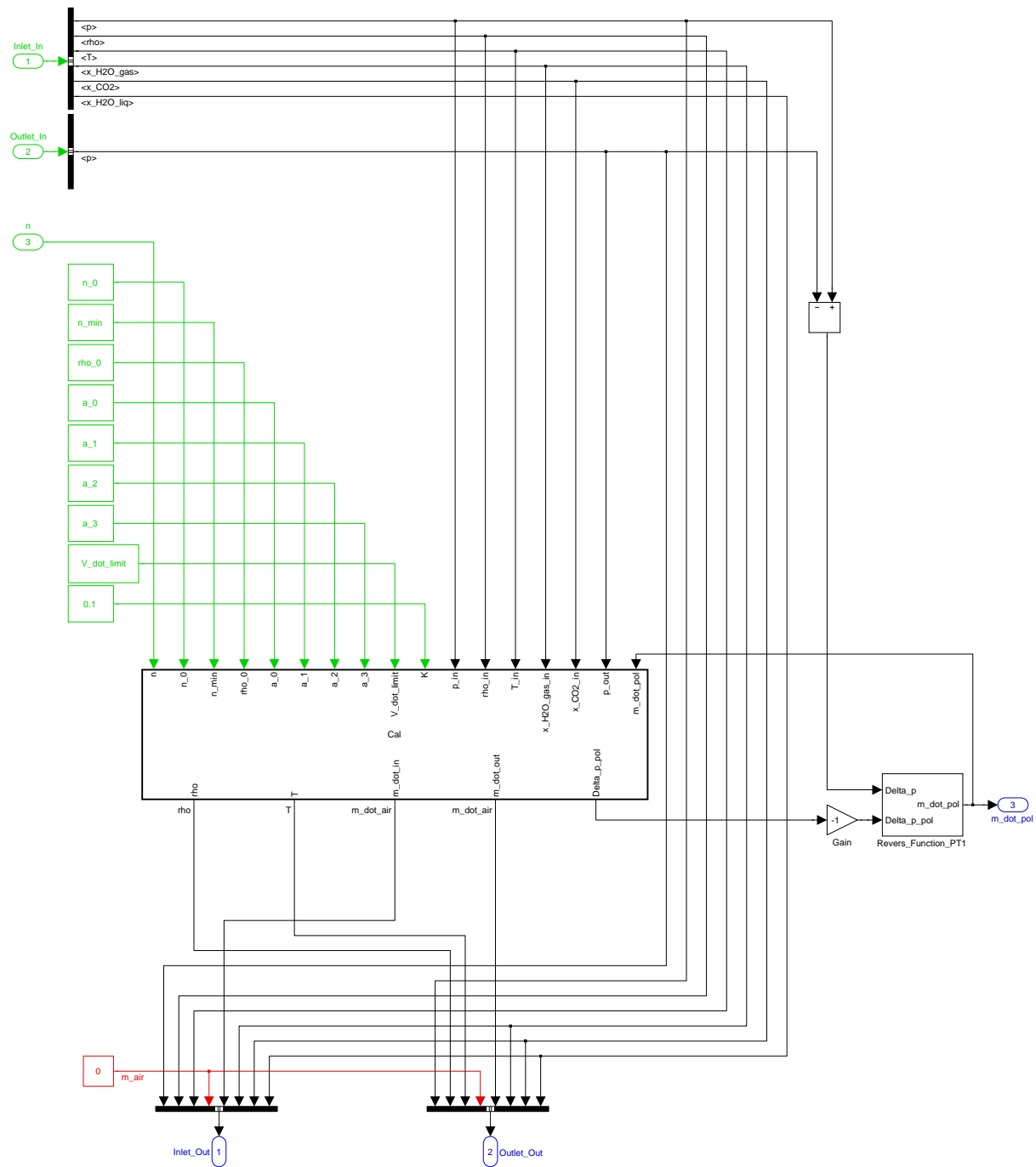
a3 [Pa/(kg/s³)]

a2 [Pa/(kg/s²)]

a1 [Pa/(kg/s)]

a0 [Pa]

V\_dot\_limit [m³/s]



```
% *****
% * Definition of a generalized fan
% *
% * Number of inputs :                3
% *
% * Parameter: Diameter:              D
% *           Reference:              n_0, rho_0
% *           Fan Curve:              a_0, a_1, a_2, a_3
% *
% *
% * Relevant input variables of Generalized_Fan
% *
% * Pressure:                        p_in
% * Density:                         rho_in
% * Temperature:                     T_in
% * Content water vapor:             x_H2O_gas_in
% * Content CO2:                     x_CO2_in
% * Content water:                    x_H2O_liq_in
% *
% *
% * Relevant output variables of Generalized_Fan
% *
% * Temperature:                     T
% * Mass flow dry air:                m_dot_air
% * Content water vapor:             x_H2O_gas
% * Content CO2:                     x_CO2
% * Content water:                    x_H2O_liq
% *
% *****
% * Embedded Matlab Function Cal:
% *
% * Calculations:
% * 1. Definition specific gas constants.
% * 2. Definition state variables.
% * 3. Calculation mass flow.
% *
% *
% FAN CURVE
% =====
% Delta_p_zero -|----->|<- volume_margin
%               |         |
% p_delta_end   -|-----E-|
%               |         |
% 0             |         |
%               |         |
% 0             |         | V_dot_end
%               |         |
%               |         | V_dot_slope
% <----- linear curve ----->|<- cubic curve -->
% *
% *
% * Last modification : 15.03.2008
% * Author : Christian Müller(HAW)
% *
```

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% *****

% * 1. Definition specific gas constants
R_air          = 287.058;
R_H2O_gas      = 461.523;
R_CO2          = 188.924;
c_p_air        = 1005;
c_p_H2O_gas    = 1870;
c_p_CO2        = 830;

R_avg          = (R_air+x_H2O_gas_in*R_H2O_gas+x_CO2_in*R_CO2)/
(1+x_H2O_gas_in+x_CO2_in);
c_p_avg        = (c_p_air+x_H2O_gas_in*c_p_H2O_gas+x_CO2_in*c_p_CO2)/
(1+x_H2O_gas_in+x_CO2_in);
c_v_avg        = c_p_avg-R_avg;
gamma_avg      = c_p_avg/c_v_avg;
% *****

% * 2. Definition state variables
rho            = rho_in*((p_out/p_in)^(1/gamma_avg));
rho_avg        = (rho_in+rho)/2;
T              = T_in*((p_out/p_in)^((gamma_avg-1)/gamma_avg));
% *****

% * 3. Calculation mass flow
Delta_p        = 0;
Delta_p_end    = 0;
Delta_p_pol    = 0;
V_dot          = 0;
V_dot_end     = 0;
m_dot_in       = 0;
m_dot_out      = 0;
d_Delta_p_d_V_dot = 0;

a_1            = abs(a_1);
a_2            = -abs(a_2);
a_3            = -abs(a_3);
A_3            = (rho_avg/rho_0)*a_3*(n/n_0)^(-1);
A_2            = (rho_avg/rho_0)*a_2*(n/n_0)^0;
A_1            = (rho_avg/rho_0)*a_1*(n/n_0)^1;
A_0            = (rho_avg/rho_0)*a_0*(n/n_0)^2;
V_dot_limit    = abs(V_dot_limit);

if n>0
    Delta_p     = abs(p_out-p_in);
    n           = max(n,n_min);

    if A_3<0
        V_dot_end_1 = (-2*A_2+sqrt((2*A_2)^2-12*A_3*A_1))/(6*A_3);
        V_dot_end_2 = (-2*A_2-sqrt((2*A_2)^2-12*A_3*A_1))/(6*A_3);
        V_dot_end   = max(V_dot_end_1,V_dot_end_2);
        Delta_p_end = A_3*V_dot_end^3+A_2*V_dot_end^2+A_1*V_dot_end+A_0;

        if Delta_p_end < 0
            Delta_p_end = 0;
        end
    end
end

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if Delta_p <= Delta_p_end
    A_max          = max(abs(A_3),abs(A_2));
    A_max          = max(A_max,abs(A_1));
    A_max          = max(A_max,abs(A_0));
    Z_A_3          = A_3/A_max;
    Z_A_2          = A_2/A_max;
    Z_A_1          = A_1/A_max;
    Z_A_0          = A_0/A_max;
    Z_Delta_p      = Delta_p/A_max
    K_1            = 3*Z_A_3*Z_A_1-(Z_A_2^2);
    K_2            = 27*(Z_A_3^2)*(Z_A_0-Z_Delta_p)-9*Z_A_3*Z_A_2*Z_A_1+2*
(Z_A_2^3);
    K_3            = 0.5*((-4*K_2+4*sqrt((K_2^2)+4*(K_1^3)))^(1/3));
    K_4            = 0.5*((-4*K_2-4*sqrt((K_2^2)+4*(K_1^3)))^(1/3));
    V_dot          = (K_3+K_4-Z_A_2)/(3*Z_A_3);
end

if Delta_p > Delta_p_end
    Delta_V_dot     = 0.1*V_dot_end;
    d_Delta_p_d_V_dot = (3*A_3*(V_dot_end+Delta_V_dot)^2+2*A_2*
(V_dot_end+Delta_V_dot)+A_1);
    d_Delta_p_d_V_dot = max(abs(d_Delta_p_d_V_dot),0.1);
    Delta_p_zero    = Delta_p_end+d_Delta_p_d_V_dot*V_dot_end;
    V_dot_virtuell  = (Delta_p-Delta_p_end)/d_Delta_p_d_V_dot;
    V_dot           = V_dot_end-V_dot_virtuell;
end

if V_dot > V_dot_limit
    V_dot           = V_dot_limit+K*log(1+(V_dot-V_dot_limit));
end

if V_dot < -V_dot_limit
    V_dot           = -V_dot_limit-K*log(1+abs(V_dot+V_dot_limit));
end

m_dot             = V_dot*rho_avg;
m_dot_in          = -m_dot/(1+x_H2O_gas_in+x_CO2_in);
m_dot_out         = m_dot/(1+x_H2O_gas_in+x_CO2_in);
V_dot_pol         = m_dot_pol/rho_avg;
Delta_p_pol       = A_3*V_dot_pol^3+A_2*V_dot_pol^2+A_1*V_dot_pol+A_0;

if V_dot_pol<V_dot_end
    Delta_p_pol     = Delta_p_end+d_Delta_p_d_V_dot*(V_dot_end-V_dot_pol);
end
end

if A_3==0
    if A_2 == 0
        V_dot_end   = 0;
        Delta_p_end = 0;
        V_dot        = 0;
    end

    if A_2 < 0
        V_dot_end   = -A_1/(2*A_2);

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Delta_p_end      = A_2*V_dot_end^2+A_1*V_dot_end+A_0;

if Delta_p_end < 0
    Delta_p_end   = 0;
end
end

if Delta_p <= Delta_p_end
    V_dot_1       = (-A_1+sqrt(A_1^2-4*A_2*(A_0-Delta_p)))/(2*A_2);
    V_dot_2       = (-A_1-sqrt(A_1^2-4*A_2*(A_0-Delta_p)))/(2*A_2);
    V_dot         = max(V_dot_1,V_dot_2);
end

if Delta_p > Delta_p_end
    Delta_V_dot   = 0.1*V_dot_end;
    d_Delta_p_d_V_dot = (2*A_2*(V_dot_end+Delta_V_dot)+A_1);
    d_Delta_p_d_V_dot = max(abs(d_Delta_p_d_V_dot),0.1);
    Delta_p_zero   = Delta_p_end+d_Delta_p_d_V_dot*V_dot_end;
    V_dot_virtuell = (Delta_p-Delta_p_end)/d_Delta_p_d_V_dot;
    V_dot          = V_dot_end-V_dot_virtuell;
end

if V_dot > V_dot_limit
    V_dot         = V_dot_limit+K*log(1+(V_dot-V_dot_limit));
end

if V_dot < -V_dot_limit
    V_dot         = -V_dot_limit-K*log(1+abs(V_dot+V_dot_limit));
end

m_dot           = V_dot*rho_avg;
m_dot_in        = -m_dot/(1+x_H2O_gas_in+x_CO2_in);
m_dot_out        = m_dot/(1+x_H2O_gas_in+x_CO2_in);
V_dot_pol       = m_dot_pol/rho_avg;
Delta_p_pol     = A_2*V_dot_pol^2+A_1*V_dot_pol+A_0;

if V_dot_pol < V_dot_end
    Delta_p_pol   = Delta_p_end+d_Delta_p_d_V_dot*(V_dot_end-V_dot_pol);
end
end
end
% *****

```